STEAM COMPRESSOR TLV

MODEL SC

STEAM COMPRESSOR THAT RECOVERS LOW PRESSURE STEAM AT HIGHER PRESSURE FOR REUSE

Features

Maximizes steam utilization by recovering excess low pressure steam at a higher pressure resulting in reduced energy costs and CO₂ emissions.

- 1. Reuses energy from excess steam by increasing it to low/medium pressure.
- 2. No electricity required, so suitable for explosionproof areas (with COS pressure control valve).
- 3. Condensate recovery tank unnecessary with optional condensate recovery package: condensate is first reduced to atmospheric pressure, then repressurized to mid-pressure steam for reuse.
- 4. Employs a new, independently-designed high efficiency ejector.
- 5. Pressure control valve has a built-in separator and steam trap, maintaining dry motive steam, thereby ensuring high long-term efficiency and stable discharge pressure.



Specifications

Model*		Steam Compressor Unit						High-capacity Steam Compressor					
Model			SC1-1	SC1-2	SC1-3	SC2-1	SC2-2	SC2-3	SC7-1	SC7-3	SC14	SC21	SC31
Pressure Control Valve			COS	CV-COS	CV10	COS	CV-COS	CV10	COS	CV10			
Motive Inlet		25 mm		50 mm		80 mm		100 mm	150 mm	200 mm			
Connection	Discharge Outlet		80 mm		100 mm		150 mm		200 mm	250 mm	300 mm		
	Suction Inlet		80 mm					100 mm		150 mm	200 mm	250 mm	
Max. Operating Pressure (MPaG) PMO		1	.6	2.0	1.6	1.0	2.0	1.6	2.0	2.0			
Motive Steam Pressure Range (MPaG)		0.6	-1.6	0.6-2.0	0.6-1.6	0.6-1.0	0.6-2.0	0.6-1.6	0.6-2.0	0.6-2.0			
Max. Operating Temperature (°C) TMO			220										
Maximum Steam Suction Capacity		n Capacity	See "Model Selection and Performance Graphs" on pages 3 and 4.										
Discharge Steam Pressure Maximum		Contact TLV**											
(Attainable Press	ure) (MPaG)	Minimum	0.1	0.0	05	0.1	0.0	05	0.1	0.05	Co	ontact TL	V**
Suction Steam Pressure Range			Atmospheric pressure or higher***										
Applicable Fluid		Steam											

 * Products exceeding specifications shown above may be able to be supplied depending on conditions.
1 MPa = 10.197 kg
** Depends on conditions such as the pressure and volume of motive steam and suction steam. See "Model Selection and Performance Graphs" on pages 3 and 4 for an approximate figure.
*** Contact TLV for cases at or lower than atmospheric pressure. 1 MPa = 10.197 kg/cm²

PRESSURE SHELL DESIGN CONDITIONS (NOT OPERATING CONDITIONS): Maximum Allowable Pressure (MPaG) PMA: Steam Compressor Unit: 1.6 (COS/CV-COS), 2.0 (CV10); High-capacity Steam Compressor: 2.0

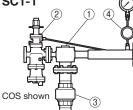
SC1-1

Maximum Allowable Temperature (°C) TMA: 220

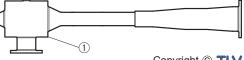


To avoid abnormal operation, accidents or serious injury, DO NOT use this product outside of the specification range. Local regulations may restrict the use of this product to below the conditions quoted.

No.	Desc	ription	Material	JIS	ASTM/AISI ¹⁾	
1	Ejector		Carbon Steel	S25C	AISI1025	
	2 Pressure Control Valve	COS	Cast Iron	FC250	A126 CI.B	
2		CV-COS	Cast Iron	FC250	A126 CI.B	
	Control valve	CV10	Cast Steel	—	A216 Gr.WCC	
3	Check Valve ^{2),}	3)	Cast Stainless Steel	—	A351 Gr.CF8	
4	Pressure Gaug	ge ⁴⁾	—	—		
(5)	Pressure Trans	smitter ^{5), 6)}	—	—	—	



SC14/SC21/SC31



¹⁾ Equivalent ²⁾ Check Valve for SC1/SC2 has screwed-in flange ³⁾ SC7 comes with connecting bolts, nuts, and gaskets ⁴⁾ COS only ⁵⁾ CV-COS/CV10 only ⁶⁾ Shown on reverse Copyright © TLV

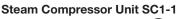


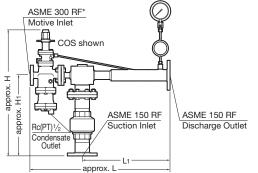
System Configuration (Steam Compressor Unit)

	Steam Compressor L	Jnit SC1/SC2/SC7	Examples of Co	nnecting Equipment*
	COS Self-actuating Control Valve • Built-in separator and steam trap • No electric instrumentation required			Non-electric Condensate Recovery Pump System Package • Steam recovery at atmospheric pressure • Explosion-proof areas
Pressure Control Valve	CV-COS Pneumatic Control Valve • Built-in separator and steam trap • High-precision control with no off-set			Flash Tank • Pressurized flash steam recovery
	CV10 Pneumatic Control Valve • High-precision control with no off-set			Condensate Recovery Pump • High pressure condensate recovery

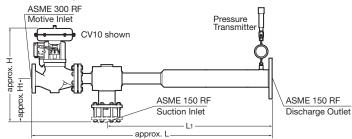
*Actual available products may differ from those shown. Contact TLV for details.

Dimensions

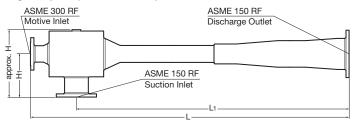




Steam Compressor Unit SC7-3



High-capacity Steam Compressor SC14/SC21/SC31



Stea	Steam Compressor Unit (mm)									
	Size	(ASME C	Class)							
Model	Motive Inlet (300RF)	Discharge Outlet (150RF)	Suction Inlet (150RF)	L	L1	Н	Ηı	Weight (kg)		
SC1-1				868		782		50		
SC1-2	25	80		000	545	862	500			
SC1-3			80	873		785		35		
SC2-1			00	1152		845		100		
SC2-2	50	100		1152	734	921	530	100		
SC2-3				1158		835		85		
SC7-1	80	150	100	1724	1140	710	300	155		
SC7-3	00	100	100	1659	1140	645	300	130		

*No ASME standard exists for cast iron; machined to fit steel flanges Other standards available, but length and weight may vary

High-capacity Steam Compressor

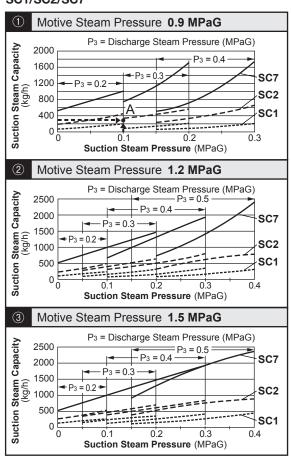
	Size	(ASME C	Class)				H1		
Model	Motive Inlet (300RF)	Discharge Outlet (150RF)	Suction Inlet (150RF)	L	Lı	Н		Weight (kg)	
SC14	100	200	150	2220	1900	475	300	240	
SC21	150	250	200	2600	2155	620	400	440	
SC31	200	300	250	3000	2500	720	450	700	

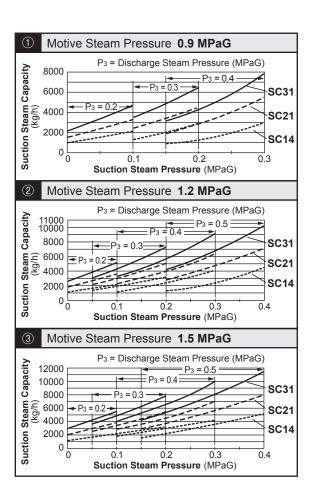
(mm)

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Model Selection Graphs

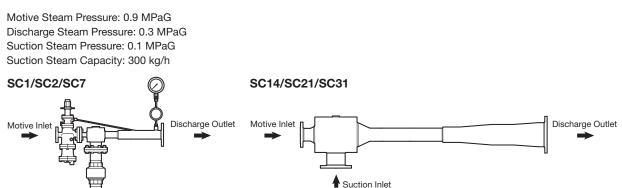
Steam Compressor Unit SC1/SC2/SC7





Model Selection

Sample Selection Conditions



Using Model Selection Graph ① for 0.9 MPaG motive steam pressure, point A represents the sample suction steam pressure and capacity conditions for the desired discharge steam pressure (P₃) of 0.3 MPaG.

In the 0.3 MPaG discharge steam pressure range, point A falls slightly below the SC2 line, therefore Model SC2 or SC7 should be chosen.

For suction steam capacities greater than that of SC31, contact TLV.

Suction Inlet

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Performance Graphs

Capacity Check (Motive Steam Quantity and Discharge Steam Quantity)

At 0.9 MPaG motive steam pressure, according to Performance Graph ①, the entrainment ratio is approximately 3.9*. The motive steam quantity and discharge steam quantity can be calculated using the formulas A) and B) below. *Entrainment Ratio = Motive Steam Quantity (kg/h) / Suction Steam Quantity (kg/h)

If motive steam pressure is between those given in Performance Graphs (1) - (3), calculate using the higher and lower pressure graphs and estimate using the mean entrainment ratio.

Sample Calculation (For motive steam pressure of 1.0 MPaG) At 0.9 MPaG motive steam pressure, according to Performance Graph ①, the entrainment ratio is approximately 3.9. At 1.2 MPaG motive steam pressure, according to Performance Graph ②, the entrainment ratio is approximately 2.8.

The calculation in C) gives an approximate entrainment ratio of 3.5.

A) Motive steam quantity = Entrainment ratio × Suction steam quantity

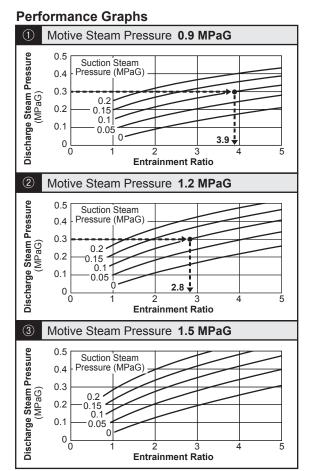
= 3.9 × 300 kg/h = 1170 kg/h

B) Discharge steam quantity = Motive steam quantity + Suction steam quantity

= 1170 kg/h + 300 kg/h = 1470 kg/h

C) Sample Calculation (For motive steam pressure of 1.0 MPaG)

 $3.9 - \frac{(1.0 - 0.9 \text{ MPaG})}{(1.2 - 0.9 \text{ MPaG})} \times (3.9 - 2.8) = 3.5$



NOTE: The type-selection and capacity values from the above procedures are only approximations. Contact TLV for actual selection and performance data.



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(M)

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